This listing of claims will replace all prior versions, and listings, of claims in the application:

Listing of Claims:

1. (Currently Amended) A process for direct conversion, by catalytic cracking, of a light olefinic hydrocarbon feed comprising at least 80% by weight of hydrocarbons containing at most 12 carbon atoms for the production of propylene, said process comprising direct cracking of the feed on a supported catalyst comprising at least one zeolite comprising silicon and aluminum and having form selectivity, from the group constituted by zeolites with one of the following structure types: MEL, ~~MFI;~~MFI, NES, EUO, FER, CHA, MFS, MWW, and from the following zeolites: NU-85, NU-86, NU-88 and IM-5, consisting of circulating the feed at a temperature in the range about 480°C to 620°C in at least one reactor on a granular moving bed of said catalyst, extracting from the lower portion of the reactor, continuously or discontinuously, a flow of catalyst comprising a carbonaceous deposit, transferring said catalyst to a regeneration zone where it undergoes at least one controlled oxidation step, then downstream of the regeneration zone, re-introducing the catalyst comprising a reduced amount of carbonaceous deposit directly or indirectly into the upper portion of said reactor, the catalyst used being such that the zeolites from said group have a Si/Al ratio in the range 40 to 130.

2. (Original) A process according to claim 1, in which at least 80% by weight of the feed is derived directly from one or more hydrocarbon cracking units.

3. (Previously Presented) A process according to claim 1, in which at least 10% by weight of the feed is derived directly from one or more Fischer-Tropsch synthesis units.

4. (Previously Presented) A process according to claim 1, in which the zeolite or zeolites of said group belong to the sub-group constituted by zeolites of structure type MEL, MFI and CHA.

5. (Previously Presented) A process according to claim 1, in which the zeolite or zeolites

of said group are of structure type MFI.

6. (Previously Presented) A process according to claim 1, in which the zeolite or zeolites of said group are constituted by ZSM-5 zeolite.

7. (Previously Presented) A process according to claim 1, in which the overall space velocity HSV is in the range 13 to $80h^{-1}$.

8. (Previously Presented) A process according to claim 1, in which the overall space velocity is in the range 33 to $60h^{-1}$.

9. (Previously Presented) A process according to claim 1, in which the residence time for the catalyst in the reaction zone is in the range 1 to 40 hours.

10. (Previously Presented) A process according to claim 1, in which the residence time for the catalyst in the reaction zone is in the range 2 to 18 hours.

11. (New) A process according to claim 9, in which the overall space velocity HSV is in the range 13 to $80h^{-1}$.

12. (New) A process according to claim 10, in which the overall space velocity HSV is in the range 13 to $80h^{-1}$.

13. (New) A process according to claim 9, in which the overall space velocity is in the range 33 to $60h^{-1}$.

14. (New) A process according to claim 10, in which the overall space velocity is in the range 33 to $60h^{-1}$.

15. (New) A process according to claim 1, wherein said granular moving bed comprises beads or extrudates having a diameter in the range of 0.6 to 4 mm.

16. (New) A process according to claim 15, wherein said granular moving bed comprises beads or extrutates having a diameter in the range of 0.4 to 6 mm.

17 (New) A process for direct conversion, by catalytic cracking, of a light olefinic hydrocarbon feed comprising at least 80% by weight of hydrocarbons containing at most 12 carbon atoms for the production of propylene, said process comprising direct cracking of the feed on a supported catalyst comprising at least one zeolite comprising silicon and aluminum and having form selectivity, from the group constituted by zeolites with one of the following structure types: MEL, MFI, NES, EUO, FER, CHA, MFS, MWW, and from the following zeolites: NU-85, NU-86, NU-88 and IM-5, consisting of circulating the feed at a temperature in the range about 480°C to 620°C in at least one reactor on a granular moving bed of said catalyst, extracting from the lower portion of the reactor, continuously or discontinuously, a flow of catalyst comprising a carbonaceous deposit, transferring said catalyst to a regeneration zone where it undergoes at least one controlled oxidation step, then downstream of the regeneration zone, re-introducing the catalyst comprising a reduced amount of carbonaceous deposit directly or indirectly into the upper portion of said reactor, the catalyst used being such that the zeolites from said group have a Si/Al ratio in the range 40 to 130.